TABLE A.5
Summary Sheet for Continuing Example 1a: Fatality Frequency Method (Method 3 of Chapter 3)

Scenario E Number 1a	Equipment Number		Scenario Title: Hexane Surge Tank Overflow. Spill not contained by the dike		
Date:		Description		Probability	Frequency (per year)
Consequence Description/Category		Release of hexane outside the dike due to tank overflow and failure of dike with potential for ignition and fatality.			
Risk Tolerance Criteria (Category or Frequency)		Maximum Tolerable Risk of a Serious Fire Maximum Tolerable Risk of a Fatal Injury			<1 × 10 <sup>-4</sup> <1 × 10 <sup>-5</sup>
Initiating Event (typically a frequency)		Loop failure of BPCS LIC. (PFD from Table 5.1)		5	1 × 10-1
Enabling Event or Condition				-	
Conditional Modifiers (if applicable)		Probability of ignition		1	
		Probability of personnel in affected area		0.5	
		Probability of fatal injury		0.5	Constant
		Others		N/A	# (F (1)
Frequency of U	nmitigate	d Consequer	nce		2.5 × 10-2
Independent Protection Layers		Dike intended to contain spill (existing) (PFD from Table 6.3)		1 × 10-2	15年6年
		SIF (to be added - see Actions)		1 × 10-2	The Section
Safeguards(non-IPLs)		Human action not an IPL as it depends upon BPCS generated alarms. Cannot be used as BPCS failure is initiating event (Approach A)			
Total PFD for all IPLs				1 × 10-4	49
Frequency of Mitigated Consequence				2.5 × 10-6	
Risk Tolerance	Criteria N	Aet? (Yes/No	: Yes, with added SIF.		
Actions Requir Meet Risk Tole Criteria		Responsible	th PFD of 1 × 10-2. Group/Person: Plant Technica ke as an IPL (Inspection, mainte		2002
Notes		Add action items to action tracking database,			
References (lin	ks to origi	nating hazar	d review, PFD, P&ID, etc.):		
References (lin LOPA analyst (			d review, PFD, P&ID, etc.): applicable):	un de la company	